

Flow Measurements for Gaseous Fuel Dispensers



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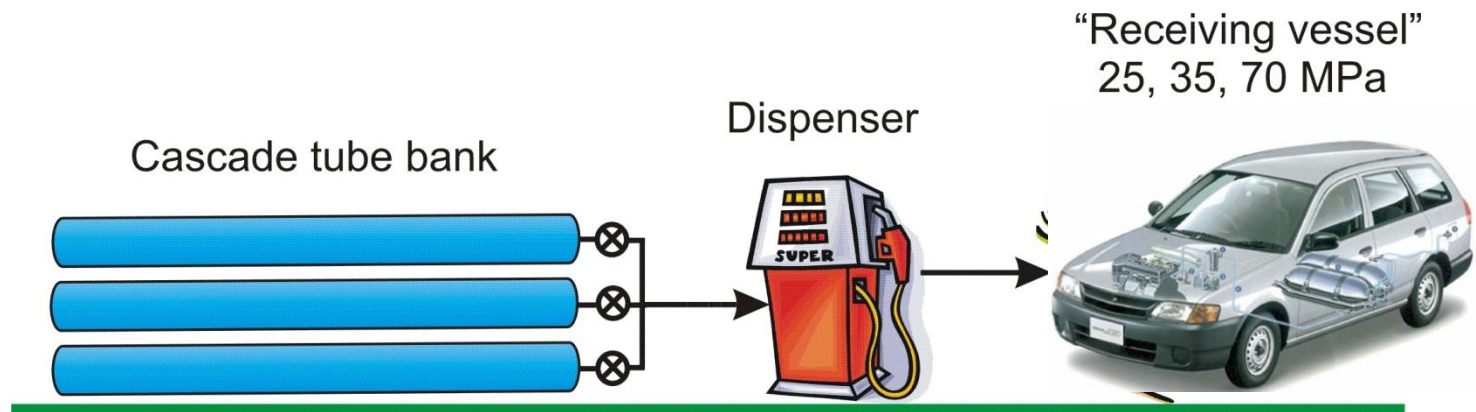
Motivation

- Gaseous fuel dispensers (H_2 and natural gas) use coriolis flow meters to bill customers

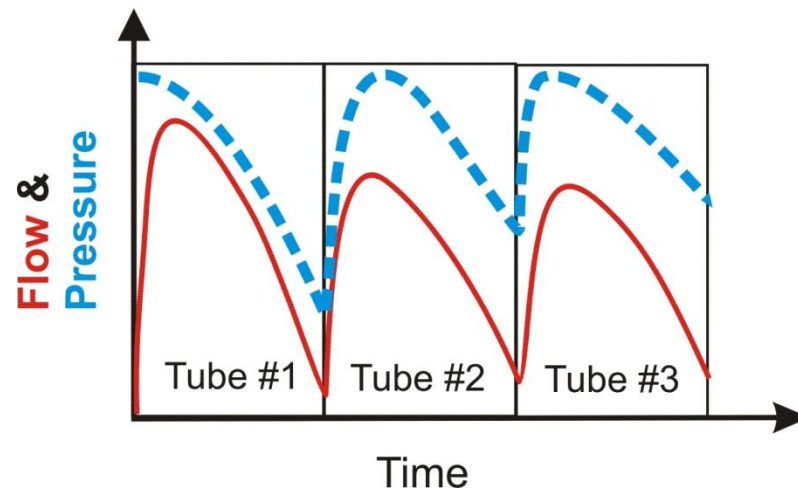


- Reported errors > 10 % due to rapidly changing pressure, temperature, and flow transients
- Regulators expect < 1.5%

Gaseous Fuel Dispenser



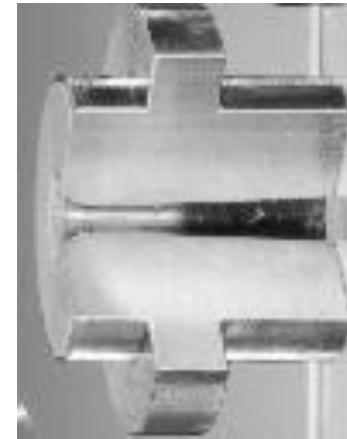
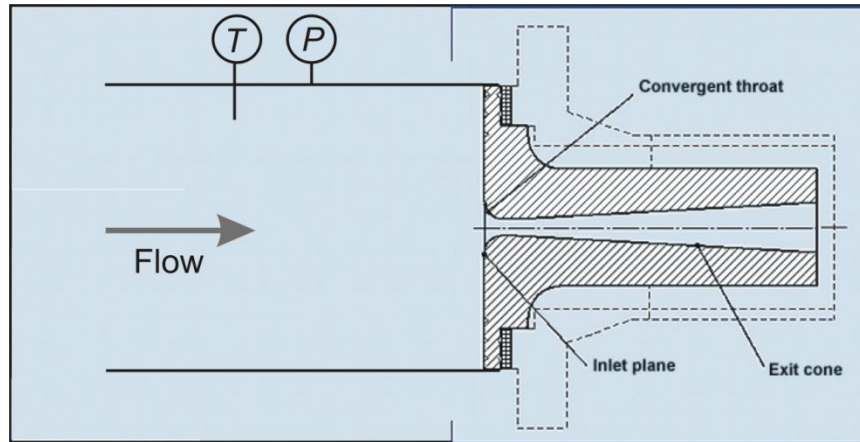
Conditions at the dispenser ...



Technical Challenge

- Find a reference flow meter with fast time response
- Construct a calibration facility to provide transient flow conditions
- Evaluate candidate dispenser flow meters

Reference Flow Meter: Critical Flow Venturi (CFV)



$$\dot{m}_{\text{CFV}} = \frac{C_d \cancel{P_0} A C^* \sqrt{\mathcal{M}}}{\sqrt{R \cancel{T_0}}}$$

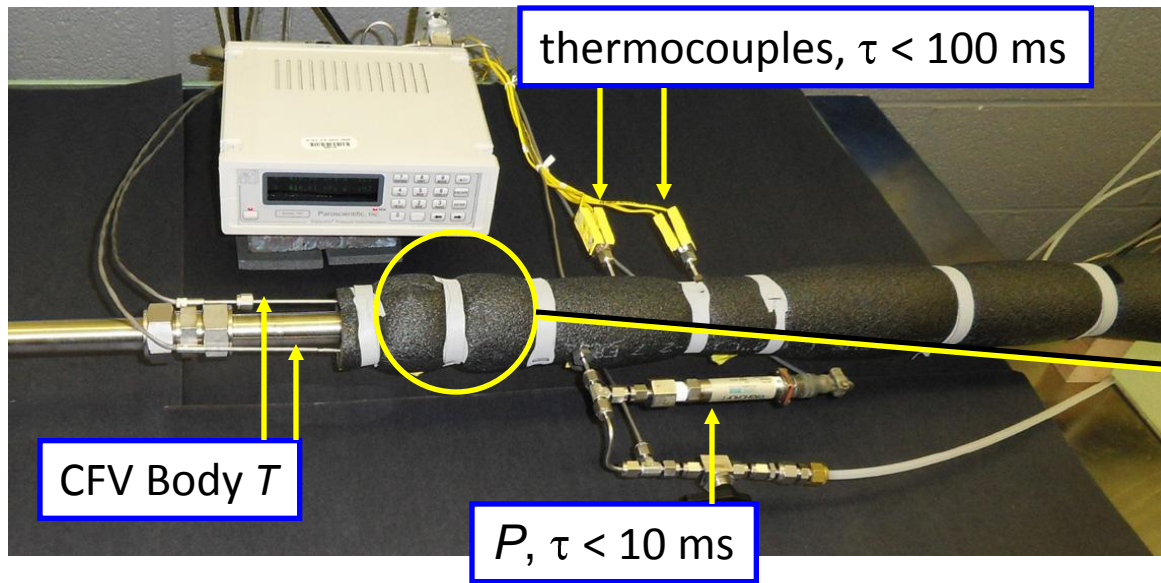
Discharge coefficient $\rightarrow C_d$
 Throat area $\rightarrow A$
 Critical flow function $\rightarrow C^*$
 Molecular mass $\rightarrow \mathcal{M}$
 Universal Gas constant $\rightarrow R$

Mass flow $\rightarrow \dot{m}_{\text{CFV}}$

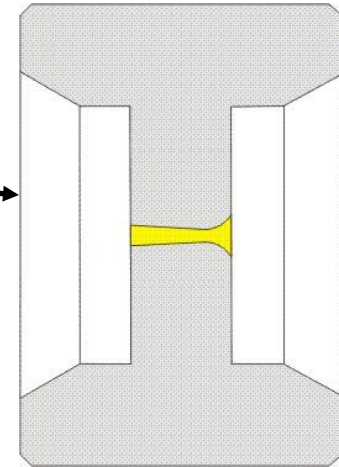
$$\tau \approx \frac{\text{length scale}}{\text{speed of sound}} = \frac{0.001 \text{ m}}{350 \text{ m/s}} = 3 \mu\text{s}$$

Pressure and temperature < 100 ms possible

Critical Flow Venturi Set-Up

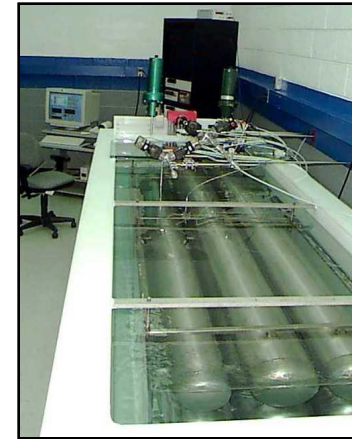
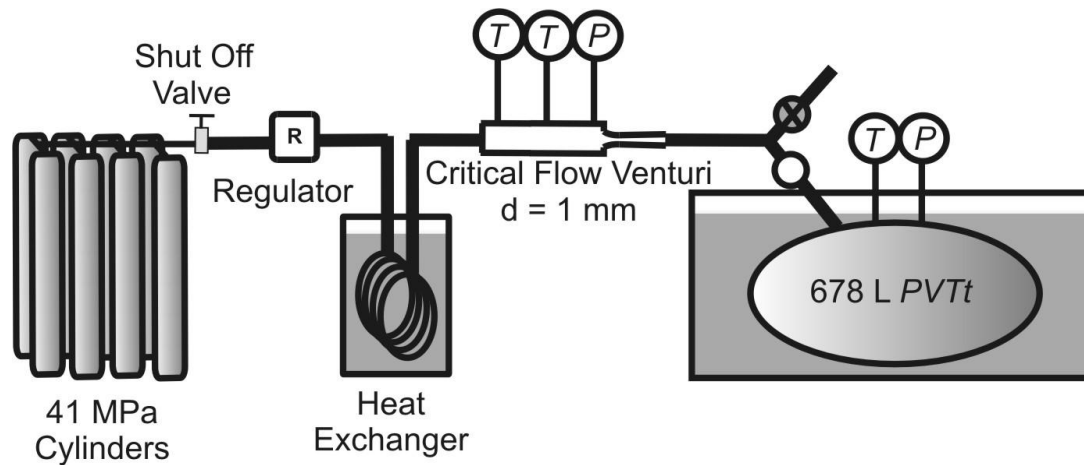


1 mm CFV in high pressure taper seal fitting

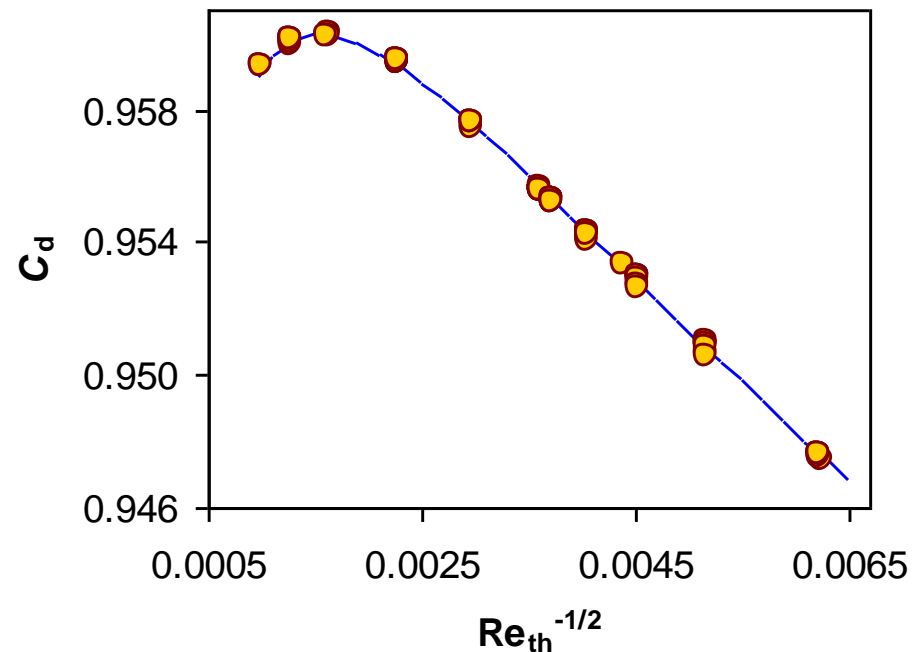


0.05 mm thermocouple pairs

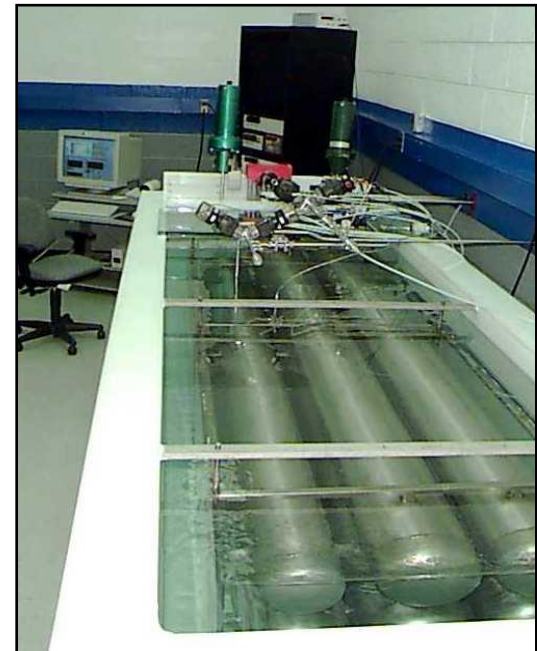
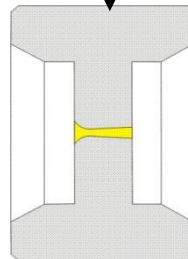
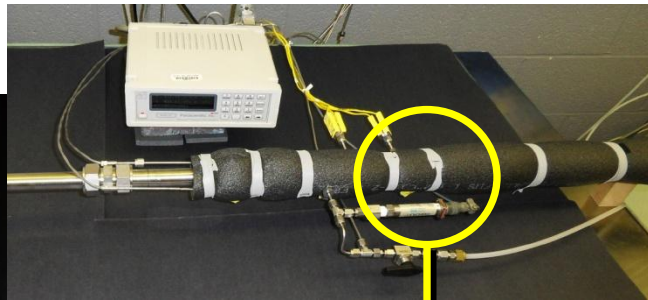
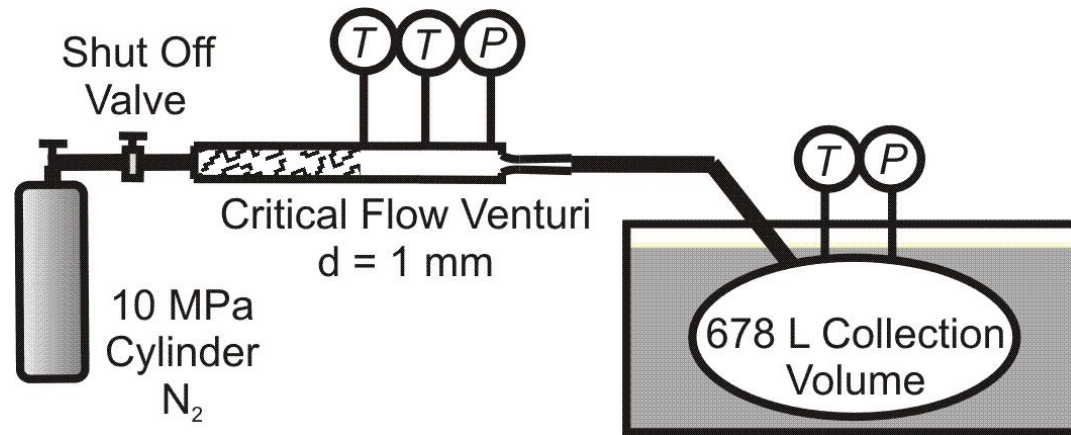
Steady State CFV Calibrations



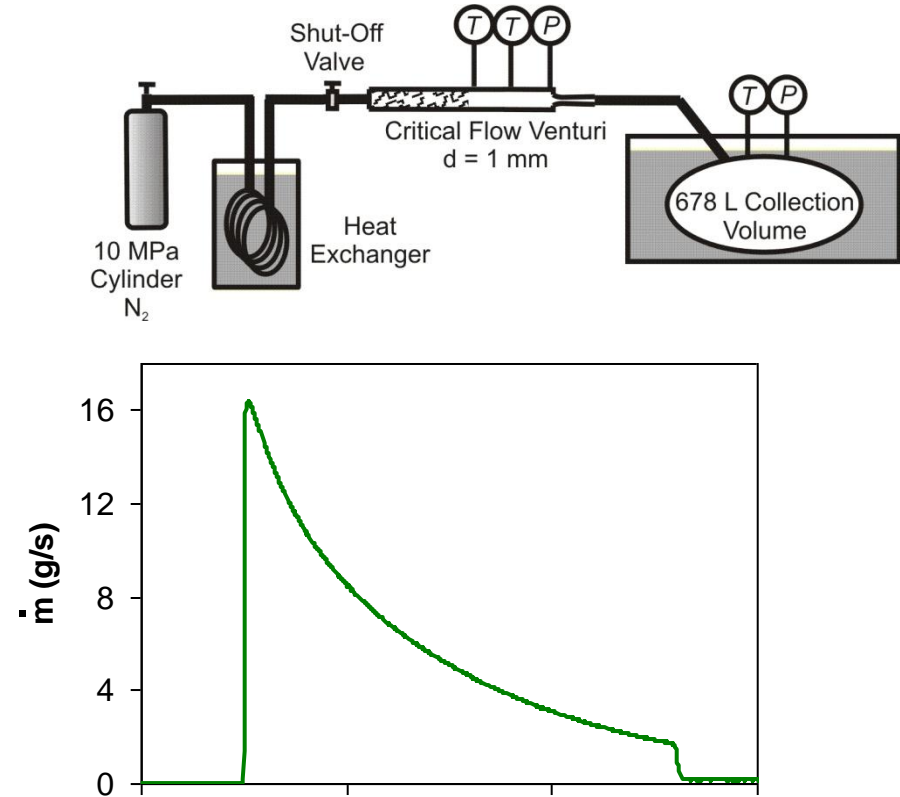
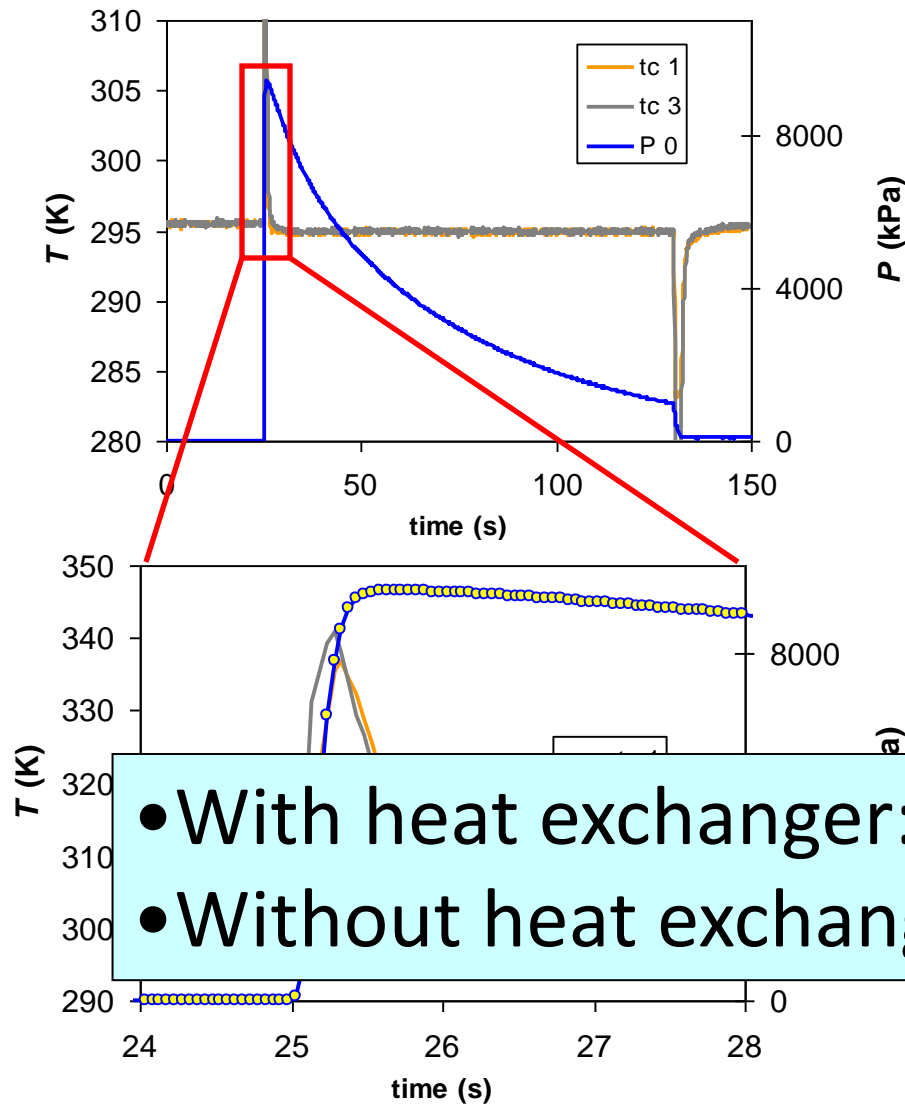
- $P_0 = 30 \text{ MPa to } 0.2 \text{ MPa}$
- Transition $Re \approx 4 \times 10^5$
- $U(C_d) = 0.07 \% (k = 2)$



Blow-Down Test

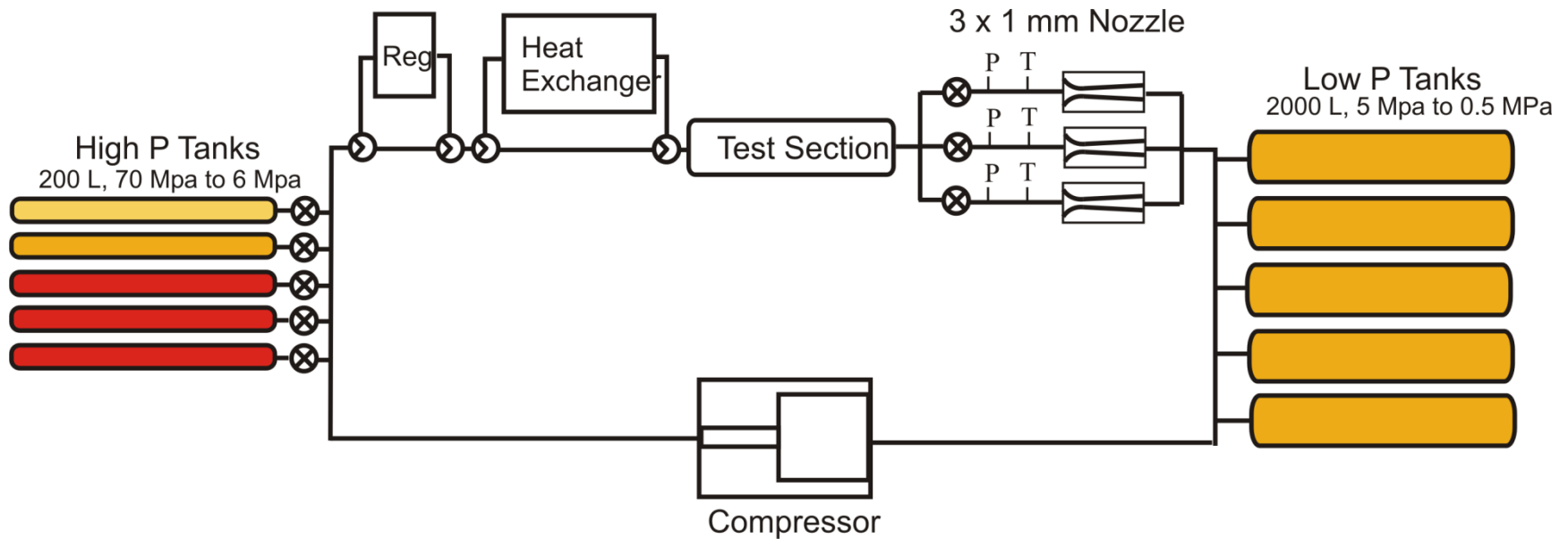
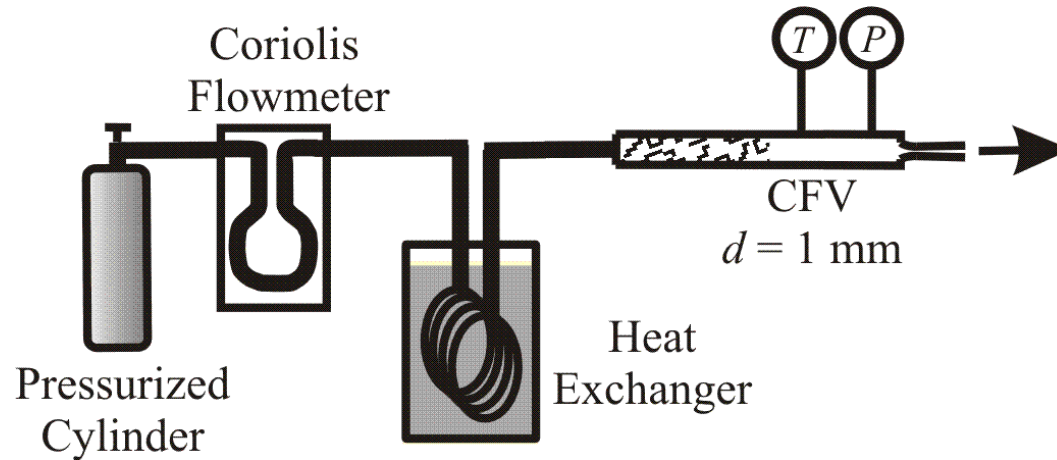


Steady State T , Transient P



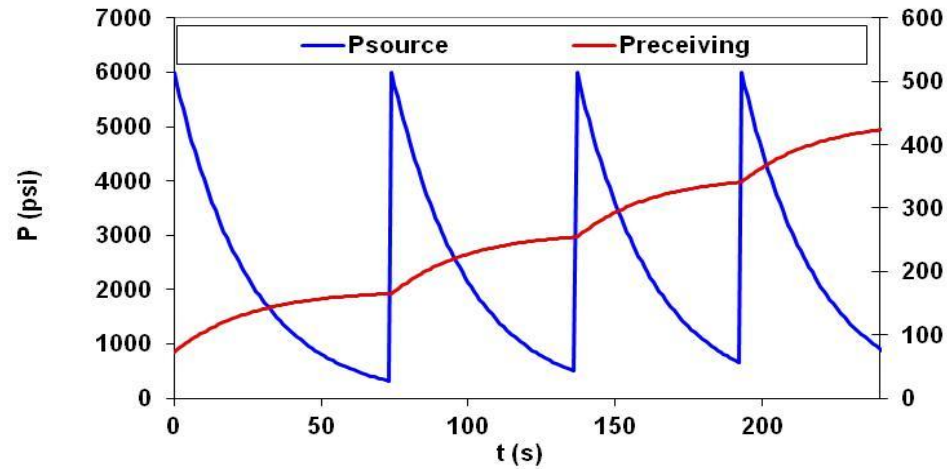
- With heat exchanger: 0.04 %
- Without heat exchanger: 0.38 % (T gradients)

Transient Flow Facility



Transient Flow Facility

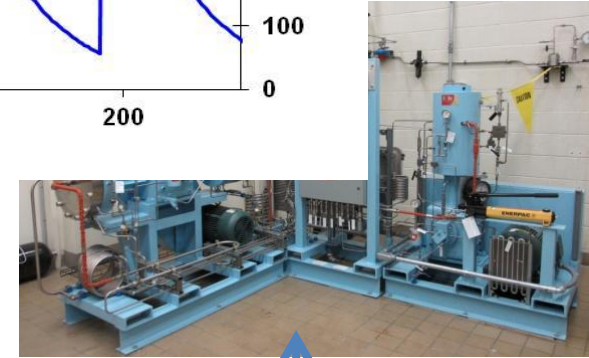
Source/Cascade Tube Bank



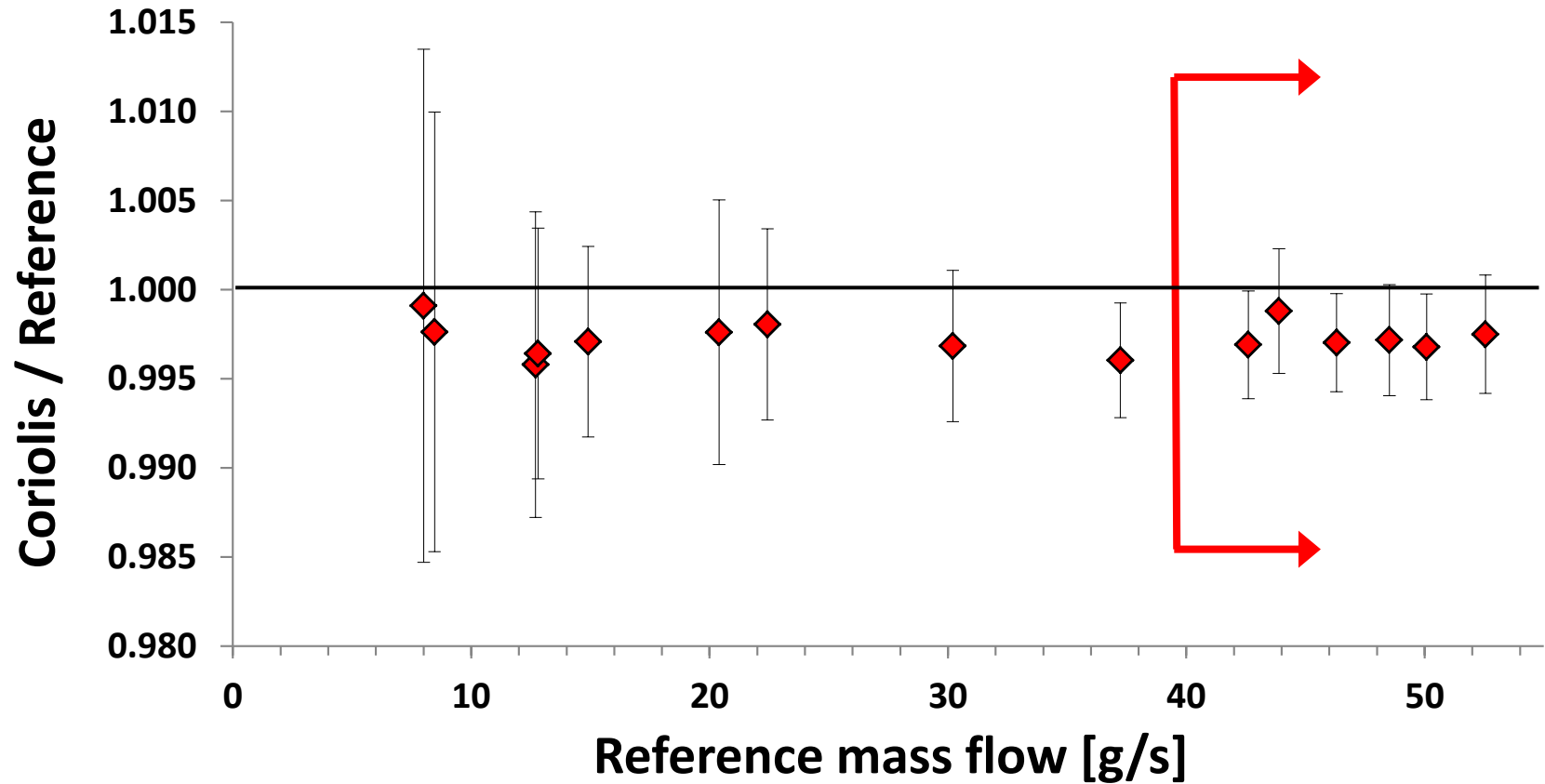
Test Bed



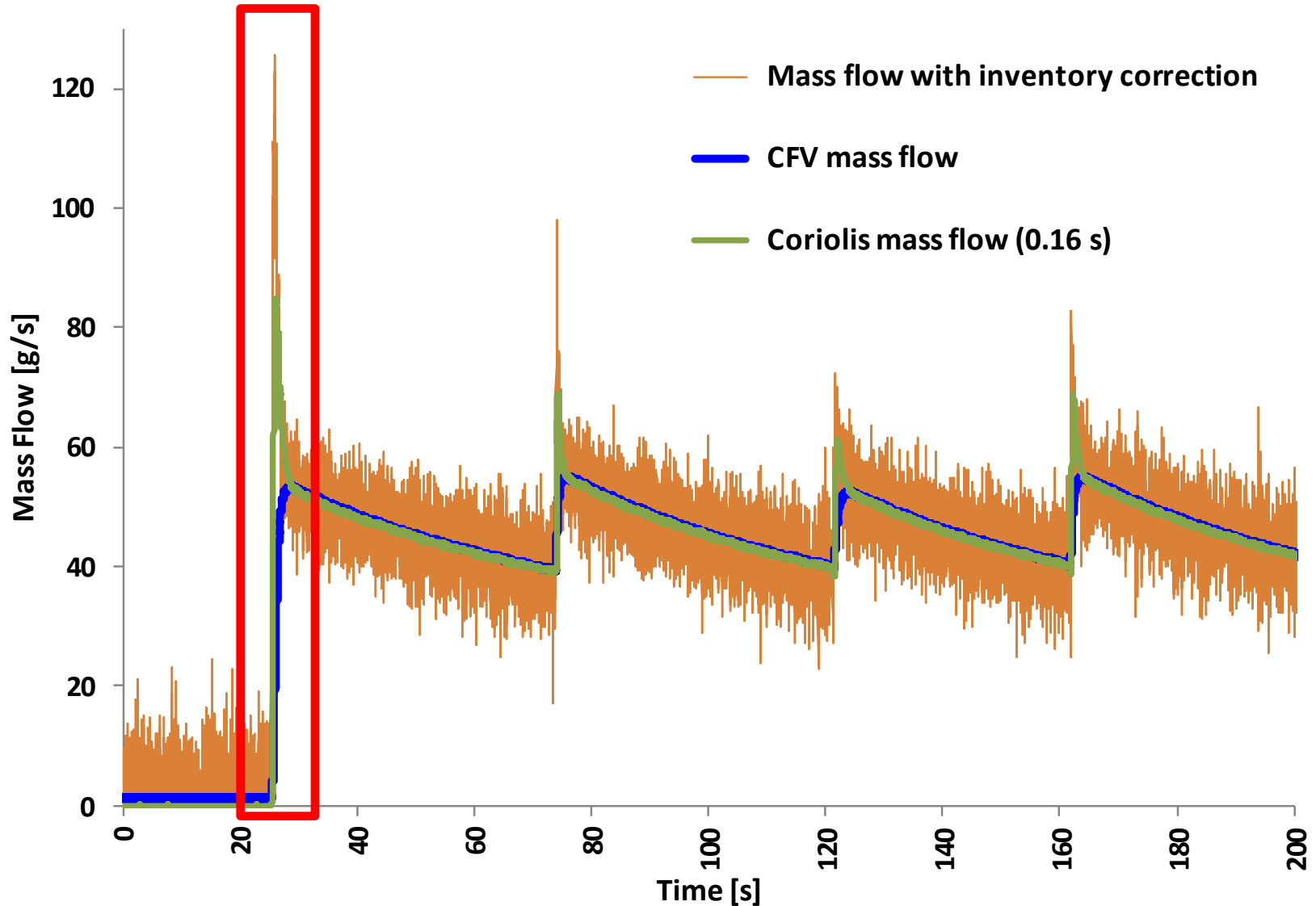
Receiving Vessel



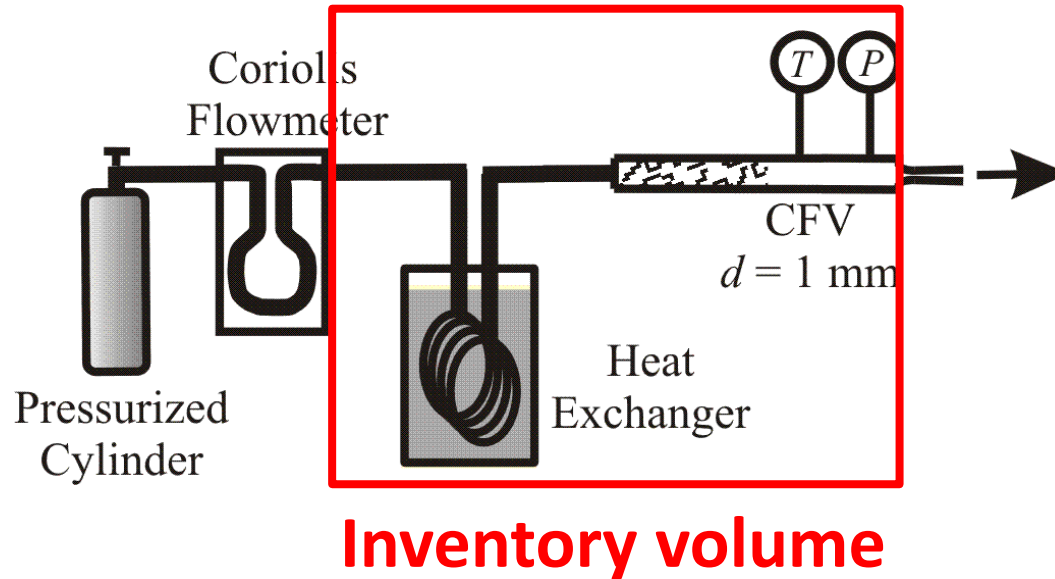
Steady State Coriolis Calibration



Simulated Cascade Fill



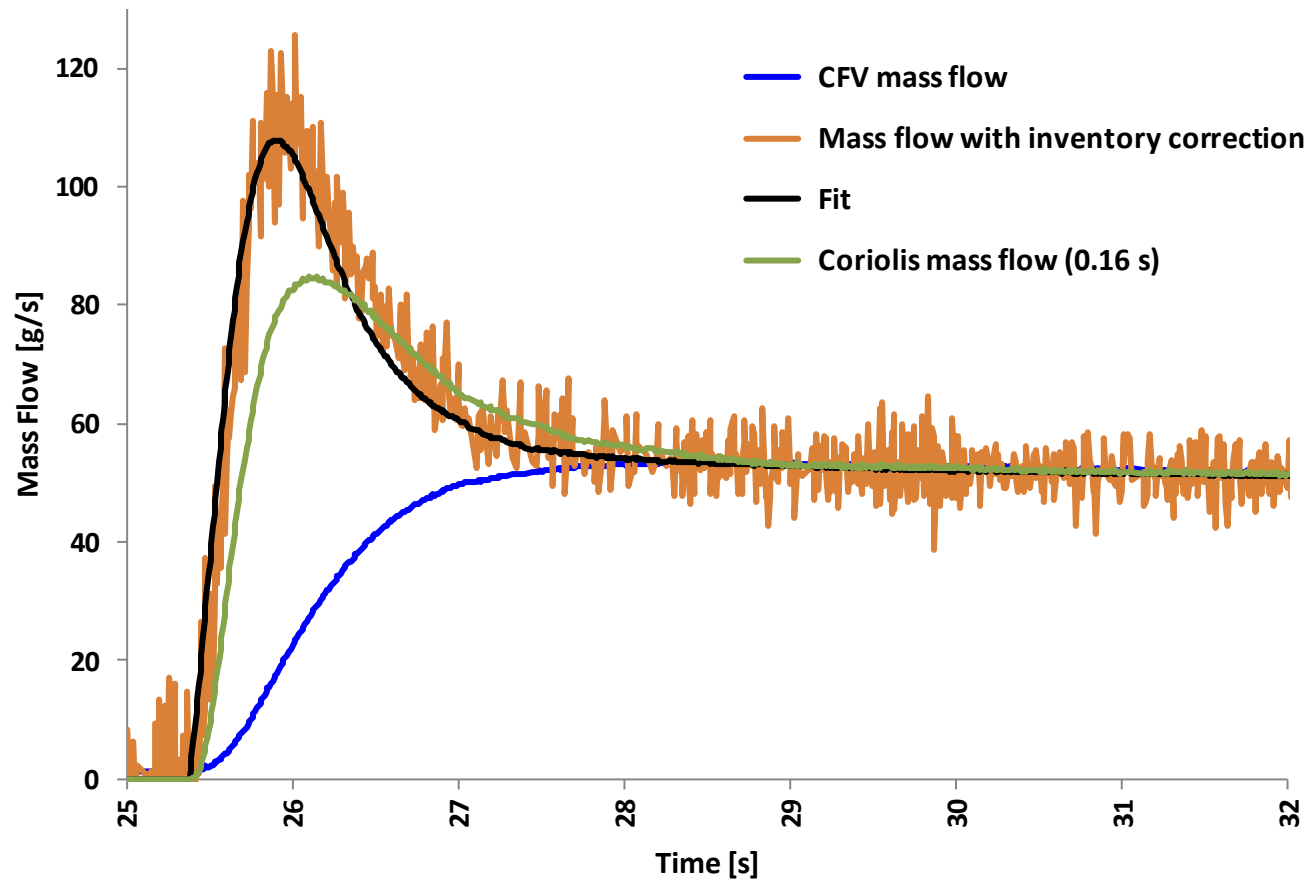
Inventory Volume Storage Effects



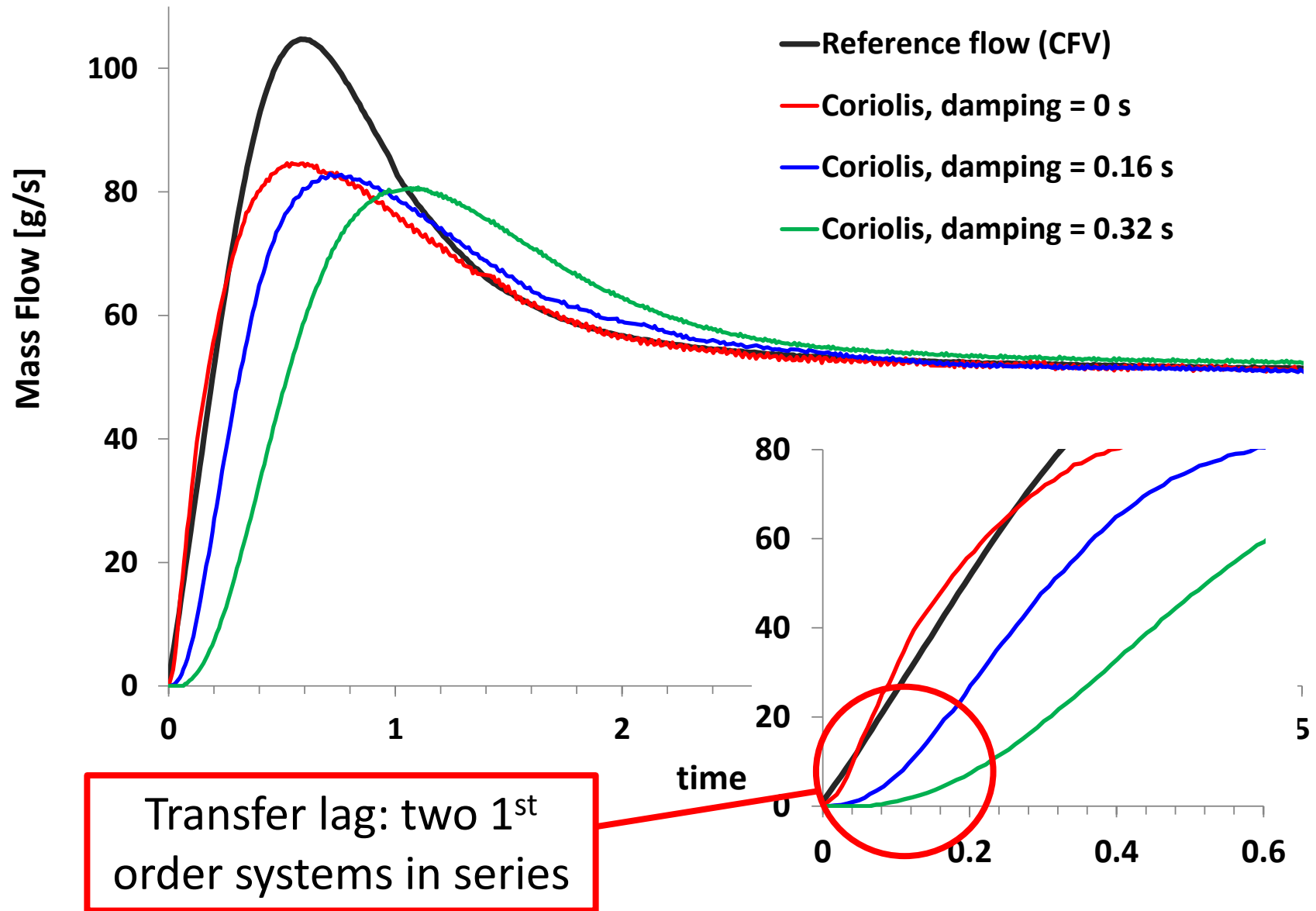
Mass balance on control volume:

$$\begin{array}{c}
 + \quad - \\
 \hline
 \sqrt{\quad} \quad \sqrt{\quad} \quad + \quad -
 \end{array}$$

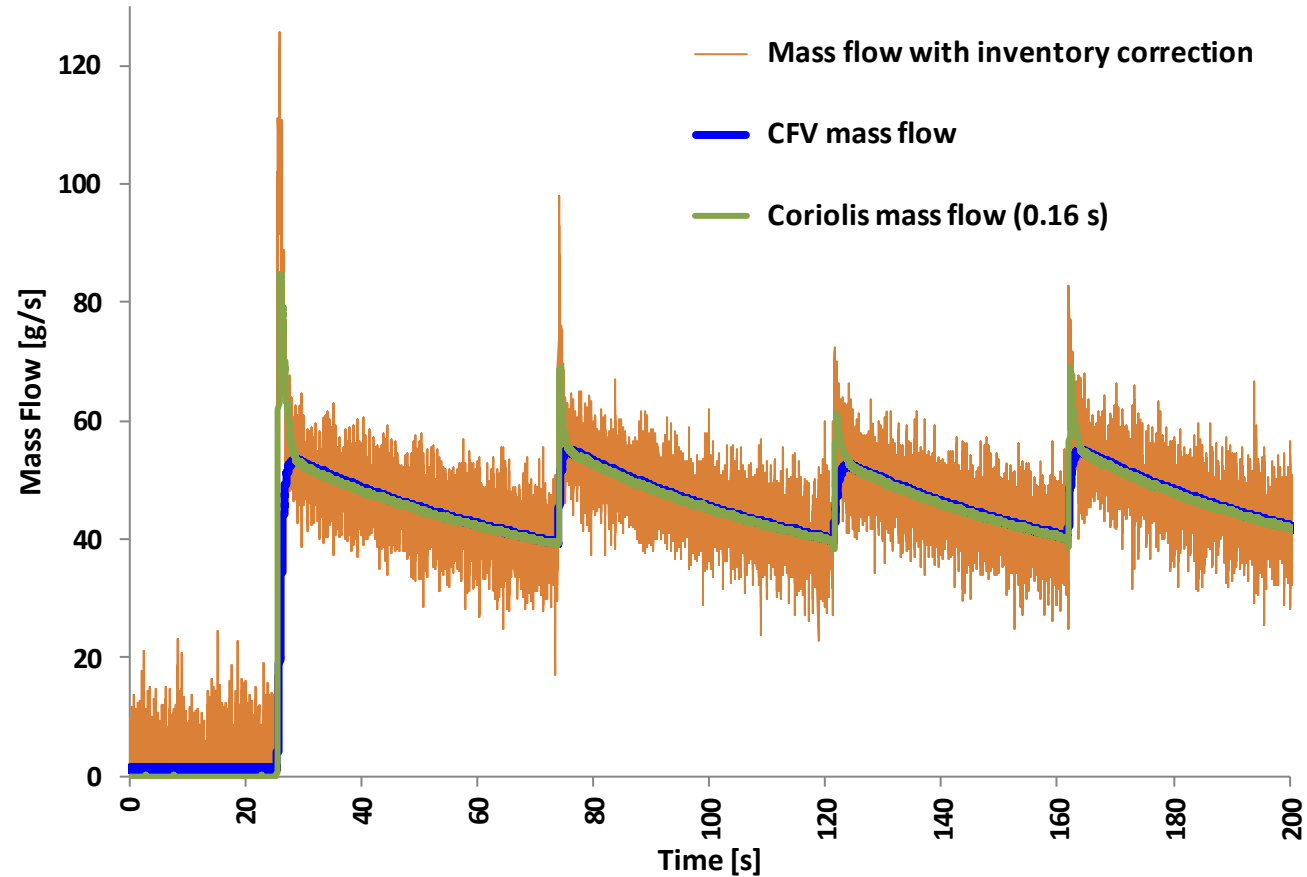
1st Transient



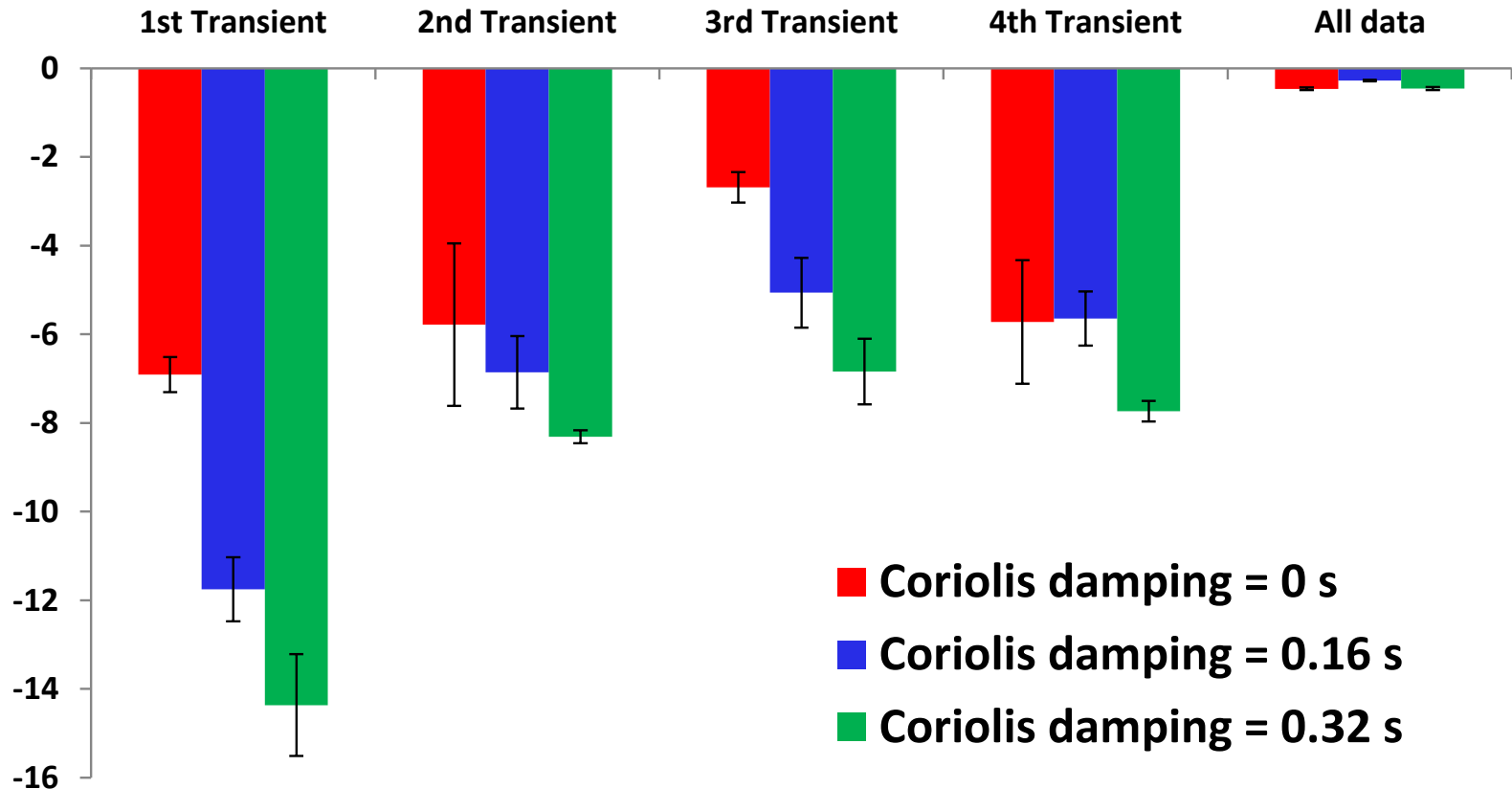
Various Coriolis Damping



Simulated Cascade Fill



% difference in totalized mass through the coriolis meter and reference CFV



Each transient: ~2 s, 100 g
All data: ~270 s, 12 kg

Uncertainty for Difference

$$\int \dot{m} dt - \Delta\rho V$$

Uncertainty Component	Normalized Sensitivity Coefficient	Uncertainty ($k = 1$, %)
A) $PVTt$ calibration		
1. $PVTt$ standard	1	0.013
2. P	1	0.020
3. T	0.5	0.010
B) CFV mass flow		
4. $C_d A$ stability	1	0.025
5. P	1	0.050
6. T	0.5	0.010
7. P and T response time	1	0.010
8. C^*	1	< 0.001
9. R , \mathcal{M}	0.5	< 0.001
C) Integration		
10. Time	1	< 0.001
11. Numerical errors	1	0.005
12. Non-critical tails	1	0.005
D) $\Delta\rho V$		
13. $\Delta\rho$	1	0.007
14. V	1	0.010
Combined Unc. ($k = 1$)		0.06
Expanded Unc. ($k = 2$)		0.13

Future Capabilities?

- Sinusoidal flow changes at frequencies up to 20 Hz
- Available gases: N₂, He,
- Increase maximum flow and pressure from 30 MPa to 70 MPa